

(19)



Europäisches Patentamt
European Patent Office
Office européen des brevets



(11) Publication number:

0 296 331 B1

(12)

EUROPEAN PATENT SPECIFICATION

(45) Date of publication of patent specification: 22.02.95 (51) Int. Cl.⁶: C08F 2/10

(21) Application number: 88106437.2

(22) Date of filing: 22.04.88

(54) High solids process for the production of water soluble polymers by exothermic polymerization.

(30) Priority: 26.06.87 GB 8715001

(43) Date of publication of application:
28.12.88 Bulletin 88/52

(45) Publication of the grant of the patent:
22.02.95 Bulletin 95/08

(64) Designated Contracting States:
DE ES FR IT NL

(56) References cited:
EP-A- 0 036 819
DE-A- 3 544 770
US-A- 4 138 539
US-A- 4 585 843

CHEMICAL ABSTRACTS, vol. 98, no. 14, April
4, 1983, Columbus, Ohio, USA SUMITOMO
CHEMICAL CO., LTD. "Apparatus for poly-
merization of acrylamide" page 18, abstract-
No. 108 032z & JP-A-57 63 305

(73) Proprietor: CYTEC TECHNOLOGY CORP.
1105 North Market Street
Suite 1300
Wilmington, Delaware 19801 (US)

(72) Inventor: Davies, William Bloor
204 Tokeneke Road
Darlen, Connecticut (US)

(74) Representative: Diehl, Hermann O. Th., Dr. et
al
Diehl & Glaeser, Hiltl & Partner
Patentanwälte
Postfach 19 03 65
D-80603 München (DE)

EP 0 296 331 B1

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid (Art. 99(1) European patent convention).

Description

The present invention relates to the process of high solids polymerization, more particularly, the process of polymerization of water-soluble polymers at high solids and particularly the use of low temperature reaction mixtures initiation in the process of high solids polymerizable.

The production of polymers at higher solids levels is desirable to provide a more efficient polymerization process, thereby increasing throughput. Until now, polymerization of water-soluble synthetic polymers such as polyacrylamide and copolymers thereof at high solids levels has been limited because of the great exothermic heat generated during polymerization. Generally, for example, the monomer content of a solution polymerization is limited to about 30% for acrylamide, for example, because of the temperature rise.

To overcome this problem, several methods have been considered. Among those proposed are a pressure process, where the reaction proceeds adiabatically and steam generation is suppressed by applying external pressure, and an evaporative process, where heat generated by the reaction is dissipated by evaporation of water from the gel. The pressure process requires exponentially increasing external pressure to suppress boiling as the solids level rises, where the evaporative process requires large surface area for the reactants (e.g. thin film or sprayed droplets).

Alternative approaches to this problem are taken in Sumitomo, Jap. Ref. 57/63,305 and Flesher, U.S. -A- 4,585,843. The Sumitomo approach involves the extraction of heat from the system during polymerization through the use of multiple heat exchange surfaces within the reactor. These cooling plates are placed in the reactor to form cavities, or subdivided sections, having thicknesses of 2-100 mm. This method is not attractive due to the very poor heat transfer from gels and the tendency for the gel to stick to the heat transfer surface. Further, the teaching of Sumitomo is not applicable to a continuous process.

The Flesher approach to high solids polymers employs a chemical heat extraction process having a salt hydrate (e.g. sodium sulfate) that undergoes an endothermic change to extract heat from the system during polymerization. The endothermic compound must be non-reactive with the monomer or monomers and resultant polymers, and in sufficient amount to counterbalance the major part of the exothermic heat of reaction. The disadvantage of this method is that the final product retains a large amount, i.e. 30-50%, of the salt.

In DE-A-3 544 770 there is described a method and an apparatus for the continuous production of polymers and copolymers of acrylic and/or methacrylic acid optionally together with further comonomers. According to the method described in this reference, an aqueous monomer solution is polymerized, whereby the monomer solution is introduced into a depression formed continuously on a continuous moving support belt. The depression shape of the support belt is being transferred continuously in a prolate flat belt shape during the polymerization of the reactants and the developing polymer gel strand is released from the belt starting from the side edges of the belt to the center portion of the belt during the transfer of the belt from its depressed to its flat shape.

The continuous production of high molecular weight water-soluble synthetic polymers in Landolt et al., U.S. 4,138,539, represents the present state of the art. This provides an improved process for preparing a water-soluble synthetic polymer in a readily dissolved powder form. The Landolt patent discloses polymerization of a monomer solution at approximately 10°C with the polymerized gel emerging at approximately 95°C by adjusting the residence time for polymerization to provide a proper combination of temperature and time to achieve the desired conversion and molecular weight. Usually a residence time of 30 to 120 minutes is considered best by Landolt. Landolt utilizes a 30 weight percent monomer solution and obtains a polymer gel generally containing 31 to 40 weight percent polymer concentration. The Landolt process is deficient however because it cannot be used to polymerize monomer solutions having higher values of monomer weight percent resulting in higher polymer concentration in the polymer gel. The heat of polymerization cannot be removed rapidly enough so lower solids solutions have to be used. In view of the limited success of high solids levels in current polymerization processes, it is, therefore, an object of the present invention to provide a process for efficient, high solids polymerization.

It is a further object of the invention to provide an efficient high solids polymerization process which can be run as a continuous as well as a batch process.

It has been discovered that higher solids levels during the exothermic polymerization of water soluble polymers can be achieved through the use of a cooled monomer solution of a syrup or a partially frozen slurry which is then initiated. In this process, a cooled syrup or slurry of monomer crystals is initiated and polymerized to produce a high solids gel. The resulting exotherm of polymerization is depressed by the sensible heat of the solution and the latent heat of fusion of the frozen part of the monomer slurry thus allowing higher solids monomer solution to be polymerized.

According to the present invention, there is provided a high solids polymerization process for producing a water soluble polymer by exothermic polymerization, said process comprising: (a) preparing a reaction mixture comprising 100 parts of exothermically polymerizable material admixed with 33 to 250 parts of water; (b) cooling said reaction mixture to a temperature of below 0°C to produce a cold high solids content mixture comprising dissolved monomer, crystals of monomer, and water; (c) polymerizing the dissolved monomer in said mixture, and (d) controlling the polymerization reaction by absorbing the heat of polymerization into a heat sink comprising sensible heat, and the latent heat of fusion of said crystals of monomer.

The sensible heat and/or heat of fusion of the cooled syrup or slurry is used to depress the exothermic T_{max} . This permits better control of the exothermic polymerization reaction.

With suitable monomers, e.g., acrylamide, partially frozen monomer slurry comprises a two phase mixture of liquid and solid monomer which leads to the production of a soluble polymer. This result is unexpected as it is known that the initiation of a solid monomer leads to an insoluble polymer.

Further, in one aspect of this invention initiation of a cooled syrup or slurry to produce high solids polymers can be used in a continuous, in-line process. The continuous process envisions using a scraped surface heat exchanger which cools the solution to a syrup or a slurry frozen phase of the monomer at the wall of a tube and a scraper which removes the cooled monomer from the wall, thereby creating a cooled solution within the tube. The monomer solution moves into the tube through a product inlet opening and the cooled syrup or slurry is moved out of the tube through the product outlet opening to complete the continuous process. Polymerization occurs outside the scraped surface heat exchanger, preferably in an advancing polymerization zone of the type shown in U.S.-A-4, 138,539.

The benefit of higher solids level polymer production is seen in energy efficiency, reducing both the cooling load and the drying load necessary in the production of a finished product. Product quality is also markedly improved because of more effective heat control.

FIGURE 1 is a cross sectional view of surface scraped heat exchanger which may be employed in the present invention.

FIGURE 2 represents a schematic drawing illustrating the important features of the process according to the preferred embodiments, with a surface scraped heat exchanger strategically located.

FIGURE 3 is a graphical plot of the exotherm T_{max} latent heat cooling as a function of time.

In one convenient manner of carrying out the process, a degassed solution of water soluble monomer at high solids concentration is introduced into a scraped surface heat exchanger and cooled to produce a partially frozen, i.e. two-phase, slurry of monomer crystals or a cooled monomer solution syrup. During the polymerization, the exothermic heat of polymerization is offset by the sensible heat of the feed as well as latent heat of fusion of crystallized monomer(s) contained in the mixture. This absorption of exothermic heat during polymerization permits higher solids levels to be polymerized.

The polymerizable material may be any polymerization monomer or prepolymer or mixture thereof which is capable of polymerization by an exothermic reaction. The polymerizable material generally comprises a polymerizable monomer, and preferably comprises one or more mono-ethylenically unsaturated monomers, especially acrylic monomers, or prepolymers formed from them. The polymer may be anionic, cationic or nonionic. Suitable acrylic monomers include (meth)acrylic acid and its salts, (meth)acrylic esters and imides, diallyldialkyl ammonium chlorides, 2-acryl-amido-2-methyl propane sulfonic acid and its salts, N-vinyl-N-methyl acetamide and allyl sulfonic acid and its salts. Preferred monomers are acrylamide, sodium acrylate, dialkylaminoalkyl (meth)acrylates, and dialkylaminoalkyl (meth)acrylamides, including quaternized derivatives of the dialkylamino compounds, for instance quaternized dimethylaminoethyl acrylate. The monomer may also be a Mannich base of acrylamide. Blends of two or more of the monomers are often preferred, so as to form copolymers and terpolymers. Other monomers that may be used include vinyl pyrrolidone and vinyl sulfonic acid and the monomers necessary to form styrene maleic anhydride copolymers or dimethylamine-epichlorohydrin polymers.

The preferred monomer comprises acrylamides alone, or in further combinations with one or more comonomers, such as acrylamide and dimethylaminoethyl methacrylate methyl chloride quaternary salt, acrylamide and sodium acrylate.

The temperature rise due to the exothermic reaction involved in the solution polymerization process limits the monomer content of the solution prepared for polymerization. In the prior art, the monomer content of a solution polymerization is limited to about 30% for acrylamide because of the temperature rise. The monomer or comonomer content of a cooled solution polymerization, on the other hand, using the process of the present invention, should be as high as possible, for example, from 35-70% by weight, and is more preferably 45-70% by weight.

A cooled syrup or slurry of monomer or comonomer crystals can be produced in various ways known to skilled in the art.

The preferred method of producing a crystal slurry or syrup of the monomer or comonomer solution is continuous and employs a scraped surface heat exchanger 2, as shown in FIGURE 1, fed with the reaction mixture. Such a heat exchanger comprises a cylindrical tube with internal rotating blades 12 which "scrape" the tube wall 10. The cooling medium is supplied to an annular jacket 14 on the outside of the tube wall 10. The monomer or comonomer solution enters through the product inlet 4 and is rotated by a shaft 6 running the length of the cylindrical tube along the cooled cylinder wall 10. As the solution moves through the cylinder, cooling occurs at the cylinder wall 10. The blades 12, affixed to rotating shaft 6, move the cooled or crystallized monomer or comonomer solution from the cylinder wall 10, mix it with the moving solution in a liquid phase to form a two phase slurry or a single phase cooled syrup and then transports the syrup or slurry out of the cylinder tube through the product outlet 8. Polymerization then occurs outside the scraped surface heat exchanger, preferably in an advancing polymerization zone, and more preferably in a continuous belt reactor.

A convenient process to polymerize the chilled reaction mixture and to isolate the polymer in useful form comprises adding from 100 to 2,000 parts per million based on the total weight of said reaction mixture of a free radical initiator; (b-1) separately preparing an aqueous redox initiator system; (b-2) mixing said redox system with said cold high solids reaction mixture while introducing said mixture into an advancing polymerization zone; (c-d) maintaining said monomer solution in said polymerization zone at suitable temperature to provide an aqueous polymer gel; (e) removing said polymer gel from said polymerization zone; and (f) granulating said polymer gel. This process, by effecting polymerization in an advancing polymerization zone, which supplies the polymer gel directly to the subsequent granulating and drying steps, eliminates the need for various equipment and handling steps associated with separate polymerization and drying procedures. It also eliminates the need for added precipitant and the deficiencies associated therewith. The process also eliminates or minimizes hydrolysis of the polymer processed. The process provides the polymer in the desired form with minimal unconverted monomer and insoluble particles.

As the free radical initiator to be incorporated in the monomer solution, use can be made of azobisisobutyronitrile, 4,t-butylazo-4'cyanovaleric acid, 4,4'-asobis(4-cyanovaleric acid and 2,2'azobis-(2-amidinopropane) hydrochloride, which is preferred. The free radical initiator should be used in effective amount which will vary depending upon the choice of monomers employed, the polymerization temperature and residence time, and other variables which preclude setting limits as to the precise quantity of free radical initiator to be used in any given case. However, it has been found that, generally, an amount corresponding to 100 to 2,000 parts per million free radical initiator based on the total weight of monomer solution to be polymerized is effective.

The redox system used as polymerization catalyst is generally one that is conventionally used. It may be based on a persulfate, for example, a system comprising potassium persulfate and sodium sulfite or on hydrogen peroxide and sodium sulfite. Preferably, ammonium persulfate and ammonium ferrous sulfate are employed. The components of the redox system are separately prepared for addition to the cold reaction mixture when the mixture is to be polymerized. The amount of redox system to be employed will also vary widely depending on various factors as indicated with respect to the free radical initiator and cannot be stated in precise quantities to cover every case. However, it has been found that in the case of the preferred system, the use of the persulfate will generally be in the range of 20-120 parts per million and the use of ferric ammonium sulfate will generally be in the range of 1-25 parts per million based on the weight of monomer.

Polymerization is conveniently done in an advancing polymerization zone through which the cold reaction mixture is transported while providing the necessary temperature and residence time to provide a polymer of the required molecular weight. The entering reaction emerges from the polymerization as a rigid gel of which the polymer generally has a molecular weight in excess of about one million, and, preferably, in excess of about ten million for preferred monomers. The mixture must enter the polymerization at a relatively low temperature of -30°C. to -10°C. and emerges at a relatively high temperature, e.g. 95°C., with the residence time being adjusted to provide the proper combination of temperature and time to achieve the desired conversion and molecular height. The actual temperature and time of polymerization will vary widely depending upon numerous factors such as choice of monomer or monomers, solution concentrations, initiator and redox system usage, feed rate of monomer solution, and other factors so that a limited specification of temperature and time cannot be given. Generally, the temperature range will vary from -30° to 100°C. over the entire polymerization zone. Preferably, the temperature peak will be in the range of 95° to 98°C. Usually, a residence time of 30 to 200 minutes is effective. When the preferred high

temperature peak range is reached, an additional residence time of 40 to 75 minutes is generally effective to provide the desired molecular weight values. The monomer solution is deoxidized prior to entry in the polymerization in accordance with conventional procedures, e.g., by blowing nitrogen through it. As a result of exposure to the polymerization reaction as described, the reaction mixture will generally lose a portion of its water content. The amount of water loss is generally small in the case where a 30 weight percent monomer solution is initially employed, the resulting polymer gel will usually contain from 31 to 40 weight percent polymer concentration. Such a loss of water has not adverse effects on processing or the polymer product.

The polymer gel obtained as described is the form of a continuous slab which enters the granulator. The slabs are granulated to provide particles having an average diameter in the range of 0.31 to 1.3 cm (1/8 to 1/2 inch) for partial drying. The slabs are readily granulated using appropriate equipment. The particle size is not especially critical and particles of the size range indicated are readily provided.

The granulated polymer gel is then dried by conventional procedures.

After the further drying step, the resulting polymer comminuted is communicated to provide a free-flowing powder which readily dissolves in water. The polymer product may be hygroscopic and accordingly, it is desirable to package the freshly ground polymer composition in moisture-proof containers to prevent cakeing during storage prior to use.

The following are examples of the present invention but are not intended nor are they to be construed so as to limit the invention in any manner whatsoever.

It is understood that many monomers and comonomers can be more efficiently polymerized by a cooling process as herein disclosed.

It is further understood that this sensible heat and latent heat extraction process can be used alone or in combination with a pressure process, an evaporative process, a chemical heat extraction process or any combination of the above.

In the Examples, the following abbreviations have the following meanings:

V50 - 2,2'-azobis(2-amidino propane) hydrochloride, a free radical initiator produced by Wako Chemicals U.S.A., Inc.

APS - ammonium persulfate, a redox catalyst component

FAS - ferrous ammonium sulfate, a redox catalyst component

Q9 - dimethylaminoethyl acrylate methyl chloride quaternary salt.

EXAMPLE 1

A batch process is carried out by initiating a slurry of cold acrylamide crystals.

Water, 122 parts by weight, V-50, 1000 parts per million by weight and APS, 100 parts per million by weight are degassed with flowing nitrogen.

The temperature of this degassed solution is reduced to 0°C and 100 parts of acrylamide crystals and 7 parts per million of FAS are added, the degassing is continued until polymerization has started. As polymerization proceeds the product is stirred as long as possible to keep the acrylamide crystals in suspension. The exotherm which initially drops on adding the acrylamide exhibits a smooth profile and reaches a T_{max} of 102°C compared with a theoretical T_{max} of 148°C for a 46% w/w solution of acrylamide (without crystals, see FIGURE 3).

| Results: | | | | | |
|---------------------|----------------|----------------------|------------|--------------|-----------------|
| PRODUCT TYPE | SOLIDS CONTENT | STANDARD VISCOSITY | INSOLUBLES | FREE MONOMER | VISCOSITY RATIO |
| Polyacryl-imide gel | 45.8% | 4.01 mPa·s (4.01 cp) | 1.5 | 0.097% | 2.3 |

EXAMPLE 2

A solution containing the ingredients given in the table below is prepared.

| Ingredients | gms |
|-----------------------------|-------|
| Acrylamide Solution (52.6%) | 337.0 |
| Deionized Water | 161.0 |
| Ammonium Chloride | 2.0 |
| Total Weight | 500.0 |
| Monomer Solids 35.4% | |

The solution is adjusted with caustic soda to pH of 6 and sparged with nitrogen for 30 minutes. The solution is then cooled (with stirring) to -7 °C at which stage the solution contains crystals in suspension. This solution is then initiated using a redox system of ammonium persulfate and ferrous ammonium sulfate. The reaction reaches a maximum temperature of 96 °C in 2 hours. After cooling, the gel is chopped and dried to form a powder with a dry weight of 94%. On analysis, the product, polyacrylamide, gives the following results:

| STANDARD VISCOSITY | INSOLUBLES |
|---------------------|------------|
| 4.3 mPa·s (4.3 cps) | 0.2% |

EXAMPLE 3

A solution containing the ingredients in the table below is prepared.

| Ingredients | gms |
|-----------------------------|-----|
| Acrylamide Solution (52.6%) | 210 |
| Q9 Monomer (77%) | 215 |
| Adipic Acid | 13 |
| Deionized Water | 112 |
| Total Weight | 550 |
| Monomer Solids 50.2% | |

The solution is adjusted with sulfuric acid to a pH of 3 and sparged with nitrogen for 30 minutes. The solution is then cooled (with stirring) to -30 °C. At this temperature the solution contains some crystals. The solution is initiated using a redox system of ammonium persulfate and ferrous ammonium sulfate. The reaction reaches a maximum temperature of 92 °C in 95 minutes. The final dry polymer is prepared in the same way as Example 2. The product analysis is:

| STANDARD VISCOSITY | INSOLUBLES | DRY WEIGHT |
|---------------------|------------|------------|
| 3.3 mPa·s (3.3 cps) | 2.0% | 91.6% |

EXAMPLE 4

Using the basic equipment depicted in Figure 2, a powdered polymer composition is prepared.

The reaction mixture is prepared at 35.4% total monomer content and consists of acrylamide. To 161 parts of water in a reactor 16, equipped with a stirrer 18, 337 kilograms of acrylamide, 52.6% in water, is added and dissolved. Finally, there are added 2.475 parts of V50 with 2.297 parts of methanol as dissolution aid therefor. The pH of the monomer solution is 7.5.

The redox system employed consists of separate aqueous solutions of ferrous ammonium sulfate and ammonium sulfate prepared in tanks 24 and 26 of the Figure. Tank 24 contains 0.26525 gram per liter of ferrous ammonium sulfate and tank 26 contains 0.75840 gram per liter of ammonium persulfate.

The usage of V50 is 721 parts per million based on the total weight of monomer. Sufficient solution of ferrous ammonium sulfate is provided to supply 6.33 parts per million based on the total weight of monomer and sufficient solution of ammonium persulfate is provided to supply 31.1 parts per million based on the total weight of monomer.

The monomer feed is metered through valve 20 to a plate and frame chiller 22 and then to a scraped surface heat exchanger 2 to chill the mixture to -7°C , then to a mixing nozzle 36 to provide a feed rate of 2.0 kilograms per minute. The redox system is simultaneously metered through valves 28 and 30 to provide the necessary parts per million of ferrous ammonium sulfate and ammonium persulfate indicated.

The supply lines of monomer solution and redox system to the mixing nozzle are designated by 33, 32 and 34 respectively. The resulting mixed solution is shown as 38 and is carried on the advancing belt 40 rotated by pulleys 42A and 42B and containing gravity take-up 44. The first pulley 42A is at a higher elevation than the second pulley 42B so that the monomer solution tends to advance toward the exit end of the polymerization zone by gravity while it remains liquid. The belt is concave across its lateral dimensions so that the monomer solution is retained within the concavity. In start-up, a dam of previously prepared gel is not necessary on the belt to prevent undue migration of the monomer solution forwardly along the belt. The belt revolves within a confined zone, not shown, with adequate provision for reaching and holding a desired polymerization temperature. Before start-up of the reaction, the monomer solution and redox system is degassed and the polymerization zone is purged with nitrogen.

The mixture of monomer solution with redox system is entered into the polymerization at a temperature of -7°C . The belt speed is such that it requires 88 seconds to travel a distance of 0.3048 m (1 foot) in linear direction, which provides a residence time of 65 minutes within the polymerization zone. At about midpoint in the polymerization zone, the formed polymer gel is at a temperature of 96°C . and this temperature is maintained the remaining distance of the advancing polymerization. In the initial portion of the polymerization, the monomer solution quickly forms a gel, the temperature rising slowly over a distance is about the first one-fourth of the polymerization zone to 40°C ., then rapidly in the second one-fourth of the zone to 96°C . The emerging gel has a polymer content of 35.4%.

The polymer gel emerging from the polymerization is conveyed to a granulator 46 which converts the slab-like polymer gel to granules having an average particle size of about 0.8 cm (about 5/16 inch) diameter. The granules are then conveyed by conveyer 48 to the partial drying oven 50 through which the granules are conveyed by means of belt 52. The dryer is maintained at a temperature of 85°C . and is equipped with a blower, not shown, which forces hot air through the gel granules. After drying for one hour in such fashion, the polymer content of the resulting partially dried gel has increased to 60%.

The partially dried polymer gel which emerges from dryer 50 is caked and the cake is broken in cake-breaker 54 and converted to dryer 56 through which they are conveyed by belt 58. The temperature of dryer 56 is also maintained at 85°C . and hot air is blown through the polymer granules by a blower not shown. After a residence time of 1.5 hours in dryer 56 the polymer granules have their moisture content reduced to 8.4%. The polymer granules emerging from dryer 56 are deposited in comminuter 60 for pulverization and emerged as a fine powder at exit port 62. The molecular weight of the dried polymer is substantially the same as that of the initial polymer gel obtained, indicating no polymer degradation occurs as a result of drying.

Many variations of the present invention will suggest themselves to those skilled in the art in light of the foregoing description. For example, the monomer composition can comprise 10% dimethylaminoethyl methacrylate and 90% acrylamide; 40% 2-vinylimidazoline and 60% acrylamide, 25% 2-vinylpyridine and 75% acrylamide, 40% dimethylaminoethyl acrylate quaternized with dimethyl sulfate and 60% acrylamide, 50% diallyldimethylammonium chloride and 50% acrylamide.

50 Claims

1. A high solids polymerization process for producing a water soluble polymer by exothermic polymerization, said process comprising:
 - (a) preparing a reaction mixture comprising 100 parts of exothermically polymerizable material admixed with 33 to 250 parts of water;
 - (b) cooling said reaction mixture to a temperature of below 0°C to produce a cold high solids content mixture comprising dissolved monomer, crystals of monomer, and water;
 - (c) polymerizing the dissolved monomer in said mixture, and

(d) controlling the polymerization reaction by absorbing the heat of polymerization into a heat sink comprising sensible heat, and the latent heat of fusion of said crystals of monomer.

2. A process as defined in Claim 1 wherein step (b) is carried out continuously in a scraped surface heat exchanger.
3. A process as defined in Claim 1 wherein steps (c) and (d) are carried out continuously and in an advancing polymerization zone.
4. A process as defined in Claim 3 wherein steps (c) and (d) are carried out in a continuous belt reactor.
5. A process as defined in Claim 1 wherein step (b) is carried out in a scraped surface heat exchanger and steps (c) and (d) are carried out in a continuous belt reactor.
6. A process as defined in Claim 1 including the steps of
(b-1) separately preparing an aqueous redox initiator system; and
(b-2) mixing said redox system with the cold high solids content mixture of step (b) prior to polymerization step (c).
7. A process as defined in Claim 6 wherein step (b-2) is carried out while introducing the cold reaction mixture continuously into an advancing polymerization zone.
8. A process as defined in Claim 1 including recovering the polymer by
(e) removing the polymer from the polymerization zone in the form of an aqueous polymer gel; and
(f) granulating and drying said polymer gel.
9. A process as defined in Claim 1 wherein the content of polymerizable material in the reaction mixture in step (a) is from 30 to 70% by weight.
10. A process as defined in Claim 1 wherein the polymerizable material comprises a monomer, alone, or in admixture with at least one comonomer and the content of said polymerizable material in the reaction mixture is from 35 to 70% by weight.
11. A process as defined in Claim 1 wherein the reaction mixture in step (a) includes from 100 to 2,000 parts per million, based on the total weight of the mixture, of a free radical initiator.
12. A process as defined in Claim 11 wherein the free radical initiator comprises 2,2'-azobis-(2-amidinopropane) hydrochloride.
13. A process as defined in Claim 1 wherein the reaction mixture comprises water and acrylamide.
14. A process as defined in Claim 1 wherein the reaction mixture comprises water, acrylamide and dimethylaminoethyl methacrylate chloride quaternary salt.
15. A process as defined in Claim 1 wherein the reaction mixture comprises, water, acrylamide and sodium acrylate.
16. A process as defined in Claim 1 wherein the polymerization reaction is controlled by step (d) in the range of from -30 ° to 100 ° C.
17. A process as defined in Claim 16 wherein the polymerization reaction is controlled in step (d) to a maximum temperature in the range of from 93 ° to 98 ° C.

Patentansprüche

1. Polymerisationsverfahren mit hohem Feststoffgehalt zur Herstellung eines wasserlöslichen Polymers durch exotherme Polymerisation, wobei das Verfahren umfaßt:

- a) Herstellung eines Reaktionsgemisches mit 100 Teilen exotherm polymerisierbarem Material, welches mit 33 bis 250 Teilen Wasser vermischt wird;
 - b) Abkühlen des Reaktionsgemisches auf eine Temperatur unter 0°C zur Herstellung eines kalten, einen hohen Feststoffgehalt aufweisenden Gemisches mit gelöstem Monomer, Monomerkristallen und Wasser;
 - c) Polymerisation des gelösten Monomers in dem Gemisch und
 - d) Steuern der Polymerisationsreaktion durch Absorbieren der Polymerisationswärme durch ein Kühlblech mit Eigenwärme und der latenten Schmelzwärme der Monomerkristalle.
2. Verfahren gemäß Anspruch 1, bei dem Schritt (b) in einem Kratzwärmetauscher kontinuierlich ausgeführt wird.
 3. Verfahren gemäß Anspruch 1, bei dem die Schritte (c) und (d) kontinuierlich und in einer fortschreitenden Polymerisationszone ausgeführt werden.
 4. Verfahren gemäß Anspruch 3, bei dem die Schritte (c) und (d) in einem Reaktor mit kontinuierlichem Band ausgeführt werden.
 5. Verfahren gemäß Anspruch 1, bei dem Schritt (b) in einem Kratzwärmetauscher und die Schritte (c) und (d) in einem Reaktor mit kontinuierlichem Band ausgeführt werden.
 6. Verfahren gemäß Anspruch 1 mit folgenden Schritten:
(b-1) separate Herstellung eines wäßrigen Redoxinitiatorsystems; und
(b-2) Vermischen des Redoxsystems mit dem kalten, einen hohen Feststoffgehalt aufweisenden Gemisch von Schritt (b) vor dem Polymerisationsschritt (c).
 7. Verfahren gemäß Anspruch 6, bei dem Schritt (b-2) während des kontinuierlichen Einbringens des kalten Reaktionsgemisches in eine fortschreitende Polymerisationszone ausgeführt wird.
 8. Verfahren gemäß Anspruch 1 mit dem Schritt der Wiedergewinnung des Polymers durch
(e) Entfernen des Polymers von der Polymerisationszone in Form eines wäßrigen Polymergels; und
(f) Granulieren und Trocknen des Polymergels.
 9. Verfahren gemäß Anspruch 1, bei dem der Gehalt an polymerisierbarem Material in dem Reaktionsgemisch in Schritt (a) im Bereich von 30 bis 70 Gew.% liegt.
 10. Verfahren gemäß Anspruch 1, bei dem das polymerisierbare Material ein Monomer umfaßt, welches allein oder mit mindestens einem Comonomer vermischt ist, und der Gehalt des polymerisierbaren Materials in dem Reaktionsgemisch im Bereich von 35 bis 70 Gew.% liegt.
 11. Verfahren gemäß Anspruch 1, bei dem das Reaktionsgemisch in Schritt (a) bezogen auf das Gesamtgewicht des Gemisches 100 bis 2000 Teile pro Million eines Initiators für freie Radikale enthält.
 12. Verfahren gemäß Anspruch 11, bei dem der Initiator für freie Radikale 2,2'-Azobis-(2-amidinopropan)-hydrochlorid enthält.
 13. Verfahren gemäß Anspruch 1, bei dem das Reaktionsgemisch Wasser und Acrylamid enthält.
 14. Verfahren gemäß Anspruch 1, bei dem das Reaktionsgemisch Wasser, Acrylamid und quaternäres Dimethylaminoethylmethacrylchloridsalz enthält.
 15. Verfahren gemäß Anspruch 1, bei dem das Reaktionsgemisch Wasser, Acrylamid und Natriumacrylat enthält.
 16. Verfahren gemäß Anspruch 1, bei dem die Polymerisationsreaktion durch Schritt (d) im Bereich von -30° bis 100°C gesteuert wird.

17. Verfahren gemäß Anspruch 16, bei dem die Polymerisationsreaktion in Schritt (d) bis zu einer maximalen Temperatur im Bereich von 93° bis 98°C gesteuert wird.

Revendications

- 5 1. Procédé de polymérisation avec une forte teneur en matières solides, pour produire un polymère soluble dans l'eau par polymérisation exothermique, ledit procédé comprenant:
 - (a) la préparation d'un mélange réactionnel comprenant 100 parties de matériaux polymérisables par voie exothermique mélangées avec 33 à 250 parties d'eau;
 - 10 (b) le refroidissement dudit mélange réactionnel à une température inférieure à 0°C pour produire un mélange froid de forte teneur en matières solides comprenant le monomère dissous, des cristaux de monomères et de l'eau;
 - (c) la polymérisation du monomère dissous dans ledit mélange; et
 - 15 (d) le contrôle de la réaction de polymérisation par absorption de la chaleur de polymérisation dans un puits thermique comprenant la chaleur sensible et la chaleur latente de fusion desdits cristaux de monomère.
2. Procédé selon la revendication 1, dans lequel l'étape (b) est réalisée en continu dans un échangeur de chaleur à couche mince.
- 20 3. Procédé selon la revendication 1, dans lequel les étapes (c) et (d) sont réalisées en continu et dans une zone de polymérisation à défilement.
4. Procédé selon la revendication 3, dans lequel les étapes (c) et (d) sont réalisées dans un réacteur à 25 courroie continu.
5. Procédé selon la revendication 1, dans lequel l'étape (b) est réalisée dans un échangeur de chaleur à couche mince et les étapes (c) et (d) sont réalisées dans un réacteur à courroie continu.
- 30 6. Procédé selon la revendication 1, comprenant les étapes consistant à
 - (b-1) préparer séparément un système aqueux d'initiateur redox; et
 - (b-2) mélanger ledit système redox avec le mélange froid à forte teneur en matières solides de l'étape (b) avant l'étape de polymérisation (c).
- 35 7. Procédé selon la revendication 6, dans lequel l'étape (b-2) est réalisée tout en introduisant le mélange réactionnel froid en continu dans une zone de polymérisation à défilement.
8. Procédé selon la revendication 1, comprenant la récupération du polymère par
 - 40 (e) élimination du polymère de la zone de polymérisation sous forme d'un gel de polymère aqueux; et
 - (f) granulation et séchage dudit gel de polymère.
9. Procédé selon la revendication 1, dans lequel la teneur en matériau polymérisable dans le mélange réactionnel de l'étape (a) est de 30 à 70% en poids.
- 45 10. Procédé selon la revendication 1, dans lequel le matériau polymérisable comprend un monomère seul ou en mélange avec au moins un comonomère et la teneur dudit matériau polymérisable dans le mélange réactionnel est de 35 à 70% en poids.
- 50 11. Procédé selon la revendication 1, dans lequel le mélange réactionnel dans l'étape (a) comporte de 100 à 2 000 parties par million, par rapport au poids total du mélange, d'un initiateur de radicaux libres.
12. Procédé selon la revendication 11, dans lequel l'initiateur de radicaux libres comprend le chlorhydrate de 2,2'-azobis(2-amidinopropane).
- 55 13. Procédé selon la revendication 1, dans lequel le mélange réactionnel comprend de l'eau et de l'acrylamide.

EP 0 296 331 B1

14. Procédé selon la revendication 1, dans lequel le mélange réactionnel comprend de l'eau, de l'acrylamide et du sel quaternaire de chlorure de méthacrylate de diméthylaminoéthyle.
- 5 15. Procédé selon la revendication 1, dans lequel le mélange réactionnel comprend de l'eau, de l'acrylamide et de l'acrylate de sodium.
16. Procédé selon la revendication 1, dans lequel la réaction de polymérisation est contrôlée dans l'étape (d) dans la gamme de -30 ° à 100 ° C.
- 10 17. Procédé selon la revendication 16, dans lequel la réaction de polymérisation est contrôlée dans l'étape (d) à une température maximum dans la gamme de 93 ° à 98 ° C.

15

20

25

30

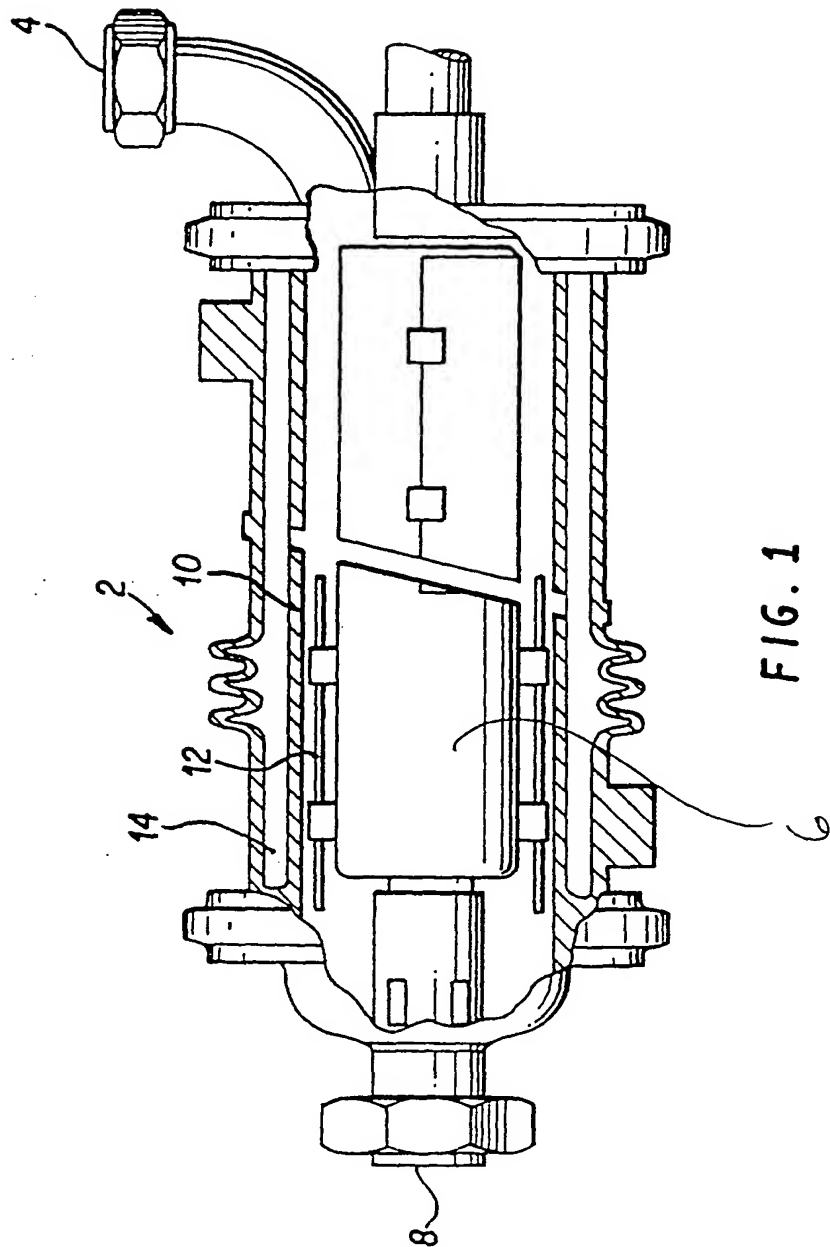
35

40

45

50

55



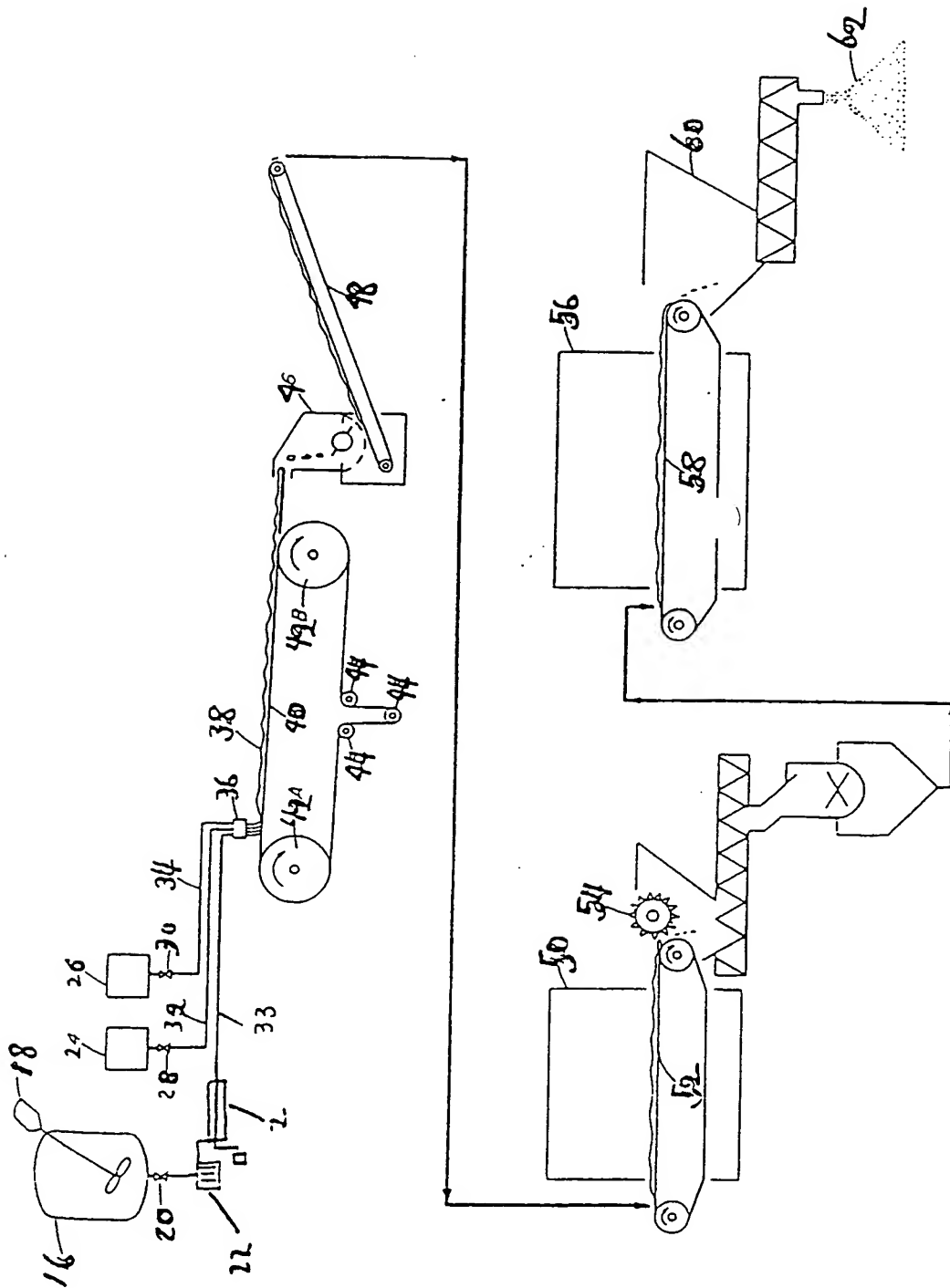


FIG. 2

